



**GIET UNIVERSITY, GUNUPUR - 765022**  
**B. Tech (Fourth Semester Regular) Examinations, May - 2024**  
**22BCHPC24001 - Chemical Engineering Thermodynamics**  
**(Chemical)**

Time: 3 hrs

Maximum: 70 Marks

(The figures in the right hand margin indicate marks)

**PART - A****(2 x 5 = 10 Marks)**Q.1. Answer **ALL** questions

	CO #	Blooms Level
a. Differentiate intensive property and extensive property giving examples.	CO1	K1
b. What is the significance of Virial coefficients?	CO2	K3
c. Write the reason behind the death of aquatic animals in summer season, through Henry's law.	CO2	K2
d. What do you mean by partial molar property?	CO2	K2
e. Write the criteria of feasibility of a chemical reaction in terms of Gibb's free energy.	CO1	K2

**PART - B****(15 x 4 = 60 Marks)**Answer **ALL** questions

	Marks	CO #	Blooms Level
2. a. Derive the expression of first law of thermodynamics for closed system.	7	CO3	K2
b. One mol of gas initially at 300 and 1000 kPa undergoes a change to 350 K and 500 kPa. Calculate the changes in internal energy and enthalpy for this process. Assume that the gas is ideal and $C_p = \frac{7}{2}R$ and $C_v = \frac{5}{2}R$	8	CO2	K3
(OR)			
c. Reported values of Virial coefficients of isopropanol vapor at 200 °C are $B = -388 \text{ cm}^3/\text{mol}$ . Calculate molar volume (V) and compressibility factor (Z) for isopropanol vap at 200 °C and 10 bar by using	7	CO2	K3
(i) Ideal gas equation			
(ii) $Z = \frac{PV}{RT} = 1 + \frac{B}{V}$			
d. Derive the expression of entropy change for ideal gas.	8	CO2	K3
3. a. Derive the expression of phase rule for intensive variables. Extend it to define both intensive and extensive variable of a system which is known as Duhem's rule.	7	CO3	K2
b. Assuming validity of Raoult's law, do the following calculations for the benzene(1)/toluene(2) system:	8	CO2	K3
(i) Given $x_1 = 0.33$ and $T = 100 \text{ }^\circ\text{C}$ , find $y_1$ and P			
(ii) Given $x_1 = 0.33$ and $P = 120 \text{ kPa}$ , find $y_1$ and T			

Vapor pressure of benzene and toluene can be calculated by Antoine equation

$$\text{For benzene, } \ln P^s / \text{kPa} = 13.7819 - \frac{2726.81}{T/K - 55.578}$$

$$\text{For toluene, } \ln P^s / \text{kPa} = 13.9320 - \frac{3056.96}{T/K - 55.525}$$

(OR)

- c. Binary system of acetonitrile (1)/ nitromethane (2) conforms closely to Raoult's law. Vapor pressures for the pure species are given by the following Antoine equations: 10 CO2 K3
- $$\ln P_1^{sat}/kPa = 14.2724 - \frac{2945.47}{T-49.15}$$
- $$\ln P_2^{sat}/kPa = 14.2043 - \frac{2972.64}{T-64.15}$$
- Given T is in K in the Antoine equation  
Prepare a graph showing P vs  $x_1$  and P vs  $y_1$  for a temperature of 75°C.
- d. Write short notes on Raoult's law for ideal solution. 5 CO1 K1
- 4.a. Derive the expression for Gibbs-Duhem theorem from partial molar properties. 7 CO3 K2
- b. Derive the Maxwell's relation from the fundamental property relations of thermodynamics. The enthalpy of a binary liquid system of species 1 and 2 at fixed T and P is represented by the equation 8 CO2 K3
- $$H = 400x_1 + 600x_2 + x_1x_2(40x_1 + 20x_2)$$
- Where H is in J mol<sup>-1</sup>. Determine expressions for  $H_1$  and  $H_2$  as a function of  $x_1$ , numerical values for the pure species enthalpies  $H_1$  and  $H_2$ , and the numerical values for the partial enthalpies at infinite dilution  $\bar{H}_1^\infty$  and  $\bar{H}_2^\infty$ .
- (OR)
- c. Derive the expression for the criteria for phase equilibrium in terms of chemical potential. 7 CO3 K2
- d. The enthalpy of a binary liquid system of species 1 and 2 at fixed T and P is represented by the equation 8 CO1 K1
- $$H = 400x_1 + 600x_2 + x_1x_2(40x_1 + 20x_2)$$
- Where H is in J mol<sup>-1</sup>. Determine expressions for  $H_1$  and  $H_2$  as a function of  $x_1$ , numerical values for the pure species enthalpies  $H_1$  and  $H_2$ , and the numerical values for the partial enthalpies at infinite dilution  $\bar{H}_1^\infty$  and  $\bar{H}_2^\infty$ .
- 5.a. Derive the expression of mole fraction in terms of reaction coordinate  $\epsilon$  for single reactions. 7 CO1 K2
- b. Consider a system in which the following reaction occur 8 CO2 K3
- $$\text{CH}_4 + \text{H}_2\text{O} \longrightarrow \text{CO} + 3\text{H}_2 \quad (1)$$
- $$\text{CH}_4 + 2\text{H}_2\text{O} \longrightarrow \text{CO}_2 + 4\text{H}_2 \quad (2)$$
- Where the numbers (1) and (2) indicate the values of j, the reaction index. If there are present initially 2 mol CH<sub>4</sub> and 3 mol H<sub>2</sub>O, determine expressions for the  $y_i$  as a functions of  $\epsilon_1$  and  $\epsilon_2$ .
- (OR)
- c. Derive the effect of temperature on equilibrium constant. 7 CO1 K2
- d. The water gas shift reaction  $\text{CO}_{(g)} + \text{H}_2\text{O}_{(g)} \rightarrow \text{CO}_{2(g)} + \text{H}_{2(g)}$  is carried out under following condition. 8 CO2 K3
- The reactants consist of 1 mol of H<sub>2</sub>O and 1 mol of CO. The temperature is 1100 K and the pressure is 1 bar. Given at 1100 K the value of  $\ln K = 0$ . Calculate the fraction of steam reacted assuming ideal gas mixture.

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