| 210 | 210 | 210 | 210 | 210 | 210 | 210 | |
|------------------------|---|---|---|--|--|--|------|
| | | | | | ation No : | Regis | F |
| B.Tech CE3I104 | D | | | | per of Pages : 02 | l Nur | Tota |
| 210 | 210 | | RANSFER - I H : CHEM, PT Marks : 100 e : 3 Hours DE : HB887 ompulsory, any | BRAN Max Tim Q.Co art-1) which is o | 210 3 Question No.1 (Pa | 210 Swer | An |
| 210 | 210 | ndicate marks. | m Part-III. hand margin i | 010 | ² The fig | 210 | |
| (2 x 10) | | | Part-I | Type Questions | only Short Answer tate Fick's Law of D | a) | Q1 |
| 210 | 210 | 210 | ture. ₂₁₀ nce nethod. | n absorption and o used in absorption wet bulb temper n Coefficient? d give its significa of McCabe Thiele ve its significance e of relative volati | ifferentiate betweer ist the equipments of efine dew point and /hat is —Distribution /rite the limitations of efine HETP and giv /rite the significance efine Tray efficience | b) c) d) e) f) g) h) i) | |
| (6 x 8) ²¹⁰ | Part-II Only Focused-Short Answer Type Questions- (Answer Any Eight out of Twelve) Ammonia gas (A) diffuses through nitrogen gas (B) under steady state conditions with nitrogen non-diffusing. The partial pressure of A at location is 1.5 x 104 Pa and that at location 2 is 5 x 103 Pa. the location 1 and 2 are 15 cm apart. The total pressure is 1.103 x 105 Pa and temperature is 298 K. calculate the flux of diffusion of ammonia. Also calculate flux of diffusion for equimolar counter diffusion assuming that nitrogen is also diffusing. Take diffusivity at prevailing conditions are 2.30 x 10-5 m2 /s. | | | | | | Q2 |
| 210 | 210 dvantages. re containing or equilibrium water to gas | 210 vantages and disa 2 from gas mixtu x can be used fo 02 kg water The | 210 raction. n terms of its adv recover 98% CO v relation y = 14 vir and x is kg C | B. 210 a for solvent in ex and packed tower b be designed to air using water. s kg CO2/ kg dry | xplain molecular di prough non ² diffusing tate selection criter compare tray tower packed tower is to 0% CO2 and 90% conditions where y is ate is kept 30% mo | b) 210 c) d) e) | |
| 210 | cal plates by ert enters the | mber of theoretic plute and rest ine re. 90% of the orig | he minimum nu ng 10 mole% sc .658 kPa pressui | ire to determine hod. s mixture contaii nperature and 10 | TU is 1 meter. tate different theorie xplain the procedu onchon Savarit met 000 m3 /h of a ga bsorber at 300 k tel emoved. Solute free | ी) g) h) | |
| | blute when it | | | | aves the tower at the | | |

| 210 | | k)]) 210 | Air (dry bulb temp. = quantity of water at 2 chamber 95% saturate bulb temperature and Briefly describe the wo | 3 °C in a spray ed. Determine th enthalpy of the e | chamber. The w e temperature, th exit air. | ater is recycled. ne relative humic | Air leaves the | 210 |
|------------|----|------------------------|--|---|---|--|---|--------------------|
| 210 | Q3 | 210 | Only Long Answer T State Fick's first law | | | | | (16) |
| | | | type flux and J-type flu | JX. | | | | |
| 210 | Q4 | 210 | A counter current pla containing 5% ammon mole NH3/mole of wa air. It is necessary to absorber at 20 0C. As (mole NH3/mole H2O) | nia by volume. Iter. The ^c scrubbe absorb 85% of t sume dilute solu | The scrubber is f er water flows at he ammonia pres tion, take Henry's | fed with water of a rate of 1 mole sent in the gas b s law constant = | ontaining 0.002 water/mole of y operating the 0.8 mole NH3 / | (16) 210 |
| 210 | Q5 | 210 | A continuous distillation methanol and 40 m methanol and water value is used? Assum moles of overhead of is at boiling point. | ole% water inte product 95 mole e relativê volatil | o an overhead e% water. Reflux ity of methanol a | product contain ratio of 2 times and water is 3. C | ing 90 mole% s the minimum Calculate¹(i) the | (16) 210 |
| | Q6 | | Two air streams are r | nived before fee | | | | <i></i> |
| | | | control. Stream 1: flo stream 2: flow rate = the enthalpy, humidity | w rate = 2kg/s, 3kg/s, temperat | temperature = 5 ure = 25 °C, rela | 50 °C, relative hi ative humidity = | umidity = 30%; 50%. Calculate | (16) |
| 210 | | 210 | control. Stream 1: flo stream 2: flow rate = | w rate = 2kg/s, 3kg/s, temperat | temperature = 5 ure = 25 °C, rela | 50 °C, relative hi ative humidity = | umidity = 30%; 50%. Calculate | (16) 210 |
| 210 210 | | 210 | control. Stream 1: flo stream 2: flow rate = the enthalpy, humidity | w rate = 2kg/s, 3kg/s, temperat and temperatur | temperature = 5 ure = 25 °C, rela e of the mixed air | 60 °C, relative h ative humidity = r stream. The tot | umidity = 30%; 50%. Calculate al pressure is 1 | |
| | | | control. Stream 1: flo stream 2: flow rate = the enthalpy, humidity atm. 210 | w rate = 2kg/s, 3kg/s, temperatur and temperatur 210 | temperature = 5 ure = 25 °C, rela e of the mixed air 210 | i0 °C, relative hi ative humidity = r stream. The tot 210 | umidity = 30%; 50%. Calculate al pressure is 1 210 | 210 |

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