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Total number of printed pages – 02

B.TECH
PCML4301

6th Semester Regular / Back Examination 2015-16

TRANSPORT PHENOMENA

BRANCH : Chemical

Time : 3 Hours

Max Marks : 70

Question Code : W554

Answer Question No. 1 which is compulsory and any FIVE from the rest.

The figures in the right-hand margin indicate marks.

Assume suitable notations and any missing data wherever necessary.

Answer all parts of a question at a place.

1. Answer the following questions : 2 x 10

- (a) Classify types of fluids in shear stress-shear strain plot only.
- (b) How viscosity and thermal conductivity depend on temperature in case of low density gases?
- (c) Define Stoke's law.
- (d) Write equation of continuity.
- (e) Define Fourier's Law of heat conduction
- (f) Specify the interface boundary condition in a system for solving heat transport problems.
- (g) State Eucken formula for thermal conductivity.
- (h) Write Fick's Law of diffusion with constant concentration.
- (i) How diffusivity varies with temperature in case of gas & liquid?
- (j) Write shell mass balance equation.

2. (a) Derive an expression for velocity profile, when Newtonian fluid flows between two vertical walls, separated by a distance $2B$, taking origin at midpoint of $2B$ distance. 06

(b) Estimate the viscosity of liquid benzene at 20°C . ($T_b = 80.1^{\circ}\text{C}$ and specific molar volume = $89.0 \text{ cm}^3/\text{g-mole}$). 04

3. (a) Derive an expression for shear stress profile, when a Newtonian fluid is flowing inside a pipe of radius R . 04

(b) One method for determining the radius of a capillary tube is by measuring the rate of flow of a Newtonian liquid through the tube. Find the radius of a capillary from the following flow data:

Length of capillary tube:	60.0 cm
Kinematic viscosity of liquid:	$4.0 \times 10^{-5} \text{ m}^2/\text{s}$
Density of liquid:	1000 kg/m^3
Pressure drop in the horizontal tube:	$5 \times 10^5 \text{ Pa}$
Mass rate of flow through tube:	$3 \times 10^{-3} \text{ kg/sec}$

06

4. (a) A heated sphere of radius R is suspended in a large container of motionless body of fluid. Show that, $Nu = \frac{hD}{K} = 2$. **06**
- (b) Write combined heat flux equation and explain each term. **04**
5. (a) Write three heat source name used in heat transport analysis. **03**
- (b) The heat generated per unit volume in a parallel plate is given by: $S_v = \mu \left(\frac{v}{b} \right)^2, \frac{w}{m^3}$ where, v is the upper plate velocity; b is the distance between two plates. Taking origin at the lower plate with boundary condition $x = 0, T = T_0$, and $x = b, q_x = 0$, show that: $T - T_0 = \frac{\mu v^2}{k} \left[\frac{x}{b} - \frac{1}{2} \left(\frac{x}{b} \right)^2 \right]$. **07**
6. A viscous fluid with temperature independent physical properties is in fully developed laminar flow through a vertical tube of radius R . At $z=0$, the fully developed flow is achieved. For $z < 0$ the fluid temperature is uniform at $T = T_1$. For $z > 0$, heat is added radially at a constant, uniform flux q_0 , at the tube surface. Make a shell energy balance to obtain the differential equation for $T(r, z)$ in the zone $z > 0$. Develop the non-dimensional differential equation in terms of the following variables: $\Theta = (T - T_1)/(q_0 R / K)$, $\xi = r/R$, $\phi = Kz / (\rho C_p v_{\max} R^2)$ **10**
7. (a) Define Prandtl, Schmidt, and Lewis numbers. **03**
- (b) A hollow solid sphere has its inner ($r = R_1$) and outer ($r = R_2$) surfaces maintained at concentrations C_{A1} and C_{A2} respectively. Obtain the expression for concentration profile in the solid at steady-state condition. **07**
8. Write short notes on any **TWO**: **5 x 2**
- (a) Equation of motion
- (b) Convection heat transfer
- (c) Types of diffusion
- (d) Importance of transport phenomena