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Total number of printed pages - 02

**B.TECH**  
**PCCH4305**

**6<sup>th</sup> Semester Regular / Back Examination 2016 - 17**

**CHEMICAL REACTION ENGINEERING**

**BRANCH : Chemical Engineering**

**Time : 3 Hours**

**Max Marks : 70**

**Question Code :Z173**

**Answer Question No. 1 which is compulsory and any FIVE from the rest.**

**The figures in the right-hand margin indicate marks.**

**Assume suitable notations and any missing data wherever necessary.**

**Answer all parts of a question at a place.**

1. **Answer the following questions :** **2 x 10**
- (a) Define rate of reaction.
  - (b) Define elementary and non-elementary reactions.
  - (c) For a reaction,  $H_2 + O_2 \rightarrow H_2O$ , what is the relation between  $-r_{H_2}$  and  $-r_{O_2}$ ?
  - (d) Under what conditions the performance of PFR is equal to that of CSTR ?
  - (e) Define mean residence time or holding time.
  - (f) Define autocatalytic reaction.
  - (g) For a reaction whose rate-concentration curve rises monotonically ( $n > 0$ ), the reactors should be connected in parallel. TRUE/FALSE. Justify.
  - (h) For which reaction kinetics if the arrangement of reactors of different volumes (CSTR/PFR-CSTR/CSTR-PFR) is altered, the conversion remains same.
  - (i) Define overall and instantaneous fractional yield.
  - (j) For autocatalytic reaction which reactor is best for lower conversion?

2. The data for the 1st order decomposition of a reaction is given below. Find the activation energy and frequency factor.

K(sec <sup>-1</sup> )	0.00043	0.00103	0.0018	0.00355	0.00717
T(K)	313	319	323	328	333

**10**

3. (a) Enzyme E catalyses the fermentation of substrate A (the reactant) to product R. Find the size of mixed flow reactor needed for 95% conversion of reactant in a feed stream (25 lit/min) of reactant (2 mol/lit) and enzyme. The kinetics of the fermentation at this enzyme concentration are given by:
- $$A \xrightarrow{\text{enzyme}} R, \quad -r_A = \frac{0.1 C_A}{1 + 0.5 C_A} \frac{\text{mol}}{\text{lit. min}}$$
- (b)  $A + B \rightarrow R, \quad r_R = 10 C_A^{1.5} C_B^{1.0}$   
 $A + B \rightarrow S, \quad r_S = 10 C_A^{2.0} C_B^{1.5}$   
 What should be the contacting pattern for maximum yield of R?
4. (a) Explain the methods of size comparison between CSTR and PFR.
- (b) Derive performance equation of CSTR in terms of space time for a second order reaction,  $-r_A = K C_A C_B$ .
5. (a) Draw the concentration profiles of A, R, and S for the parallel reactions,  $A \xrightarrow{10} R, \quad A \xrightarrow{5} S$ .
- (b) Derive an expression relating conversion and space time, for N number of equal size reactors in series for 1st order irreversible reaction.
6. Derive an expression for  $C_{Rmax}$ , for a series reaction,  $A \xrightarrow{K_1} R \xrightarrow{K_2} S$ , assuming the reactions are all first order.
7. (a) Explain how to find final conversion for a known kinetics graphically, when three different volume CSTRs operate in series.
- (b) The concentration readings represent a continuous response to a pulse input into a closed vessel which is to be used as a chemical reactor. Calculate the mean residence time of fluid in the vessel, and tabulate E for the plot of exit age distribution.
- |                                  |   |   |    |    |    |    |    |    |
|----------------------------------|---|---|----|----|----|----|----|----|
| <i>t, time</i>                   | 0 | 5 | 10 | 15 | 20 | 25 | 30 | 35 |
| <i>C<sub>pulse</sub>, gm/lit</i> | 0 | 3 | 5  | 5  | 4  | 2  | 1  | 0  |
8. Write short notes on any TWO:
- (a) Batch reactor  
 (b) Plug flow reactor  
 (c) Continuous stirred tank reactor  
 (d) Recycle reactor

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