Regi	istration No.											
												_
Total Num	ber of Pages :	03									B.T. PCE5	
	5 ^t	th Sem	ester l	slunas	r Fyai	minati	on 20 [,]	17-18			I CL3	110
210	210	OCIII		nsport				1240 10		210		
				BRANC			4					
			-	Time:								
				Max Ma	_	_						
			_	estion)					
Answ	er Question N	o.1 an	•					anv f	our fro	om the	rest.	
			in the									
210 A	ssume suitab									essary	<i>/</i> .	
			er all pa		-	_				,		
Q1.	Answer the fol	lowina	auesti	ons :							(2)	x10
(a)	In Fourier's law				nstant	is calle	d the				\	
. ,	i. Stefan-E	Boltzma	ın const	ant								
	ii. Thermal		•									
210	iii. Heat tra		210	nt	210			210		210		
	iv. Thermal		-									
(b)	Prandtl number		•									
			ivity x N			•						
			fusivity				•					
			fusivity/			•						
(c)	iv. Ther In natural conve		fusivity				arame	tar is				
		shoff nu		isici, ili		iatii ig p	aranie			040		
210		ert num			210			210		210		
		etz num										
	iv. Bond	d numb	er									
(d)	The rate of hea				ct of o	verall h	neat tra	ansfer (co-effic	ient, th	e	
	difference in ter	• .		the								
		selt nur										
		transfe										
210		ing volue of the			210			210		210		
(e)	The velocity pro			flow th	rough :	nine i	s					
(-)		rithmic			.oug	, p.po						
		bolic										
	iii. linea	ır										
		erbolic										
(f)	The ratio of av					aximur	n velo		case of		ar	
210	flow of a Newto	nian flu	iid in a d	circular	pipe is			210		210		
	ı. 1 ii. 2											
	iii. 2											
	iv. 0.5											
(g)	For a particle	settling	in wa	ter at i	ts term	inal se	ettling	velocity	, whic	h of th	e	
(3)	following is true						3	- 7				
	i. Drag	ງ = weiឲ្	ght									
210	-		yancy +	_				210		210		
	iii. Buoy	/ancy =	weight	+ drag								
	iv. Weig		uoyancy									

(h)	Where does the maximum stress occur in case of laminar flow of incompressible fluid in a closed conduit of diameter 'd'? i. At d/4 from the wall ii. At the wall					
²¹⁰ (i)	iii. At the centre iv. At d/8 from the wall The movement of molecules from an area of high concentration to an area of low concentrationis known as i. Osmosis ii. Isotonic iii. Diffusion iv. Solution As molecules diffuse, they create this, which is a difference in concentrations		2			
210	i. Concentration gradient ii. Diffusion iii. Semi-permeable iv. Osmosis		21			
	Answer the following questions:	(2x10)				
(a) (b) (c) (d) (e)	Define momentum, thermal, and mass diffusivities. Define combined momentum flux. 210 210 210 210 State Newton's Law of Viscosity with mathematical expression. What is friction factor? How thermal conductivity depends on temperature in case of low density gases		2'			
(f) (g)	and liquids? Define mass transfer co-efficient. Write the formula for overall heat transfer coefficient for a composite wall consisting of four different layers with different thermal conductivities with different thicknesses. 210 210 210 210 210		2'			
(h) (i) (j)	How diffusivity of liquids is varied with temperature? State Fick's Law of binary (molecular) diffusion. Write the unit and dimensions of momentum, thermal, and mass diffusivities.		_			
(a) (b) (c)	Explain the classification of fluids. Define Stoke's law and its range of applicability. Derive an expression for average velocity profile of Newtonian fluid flow between two vertical walls separated by a distance 2B, taking origin at midpoint of 2B distance.					
(a)	What pressure gradient is required to cause di-ethylaniline $(C_6H_5N(C_2H_5)_2)$, to flow in a horizontal, smooth, circular tube of inside diameter D=3cm at a mass rate of 1028 gm/sec at 20 $^{\circ}$ C? At this condition, density of di-ethylaniline is 0.935 gm/cm ³ and viscosity is 1.95cP. Friction factor is 0.0063.	(5)				
₂₁₀ (b)	Derive an expression for maximum velocity when a Newtonian fluid is flowing through a pipe of radius R vertically downward. Draw the velocity profile.	(10)	2'			
(a)	A heated sphere of radius R is suspended in a large motionless body of fluid. It is desire to study the heat conduction in the fluid surrounding the sphere in the absence of convection. Set upthe differential equation describing the temperature T in the surrounding fluid as a function of r, the distance from the centre of the sphere. The thermal conductivity of K of the fluid is considered constant. Integrate the differential equation and use these boundary conditions	(10)				
210	to determine the integration constants: at $r=R$, $T=T_R$ and $r=\infty$, $T=T_\infty$. From the temperature profile, obtain an expression for the heat flux at the surface. Equate this result to the heat flux given by 'Newton's Law of Cooling'		2			

Q2.

Q3.

Q4.

Q5.

	hD		
	and show that Nusselt number, $Nu = \frac{hD}{K} = 2$, in which D is the sphere		
(b)	diameter. Explain Free and Forced convection.	(5)	
Q6. 210(a)	Derive an expression for determining the mass flux of a liquid, diffusing through a stagnant gas film where the gas is non-diffusing.	(10)	210
(b)	What are the boundary conditions used for solving shell mass balance equation?	(5)	
Q7. 210	Consider a long cylindrical nuclear fuel rod, surrounded by an annular layer of aluminum cladding. Within the fuel rod heat is produced by fission; this heat source depends on position approximately as, $Sn=S_{no}\times r_{>0}^2$ where S_{n0} is known constants, and r is the radial coordinate measured from the axis of the cylindrical fuel rod. R_F and R_C are the radius of fission and cladding materials. Derive an expression for temperature profile in the cladding material if the temperature at the outer surface of cladding is T_0 .	(15)	210
Q8. 210	A droplet of liquid A of radius r_1 , is suspended in a stagnant film of gas of radius r_2 . Boundary conditions are $r = r_1$, $x_A = x_{A1_{311}}$ and $r = r_2$, $x_A = x_{A2_{21}}$. Taking the value of constant as $r_1^2 N_{Ar1}$ show that $N_{Ar1} = \frac{CD_{AB}}{r_2 - r_1} \left(\frac{r_2}{r_1}\right) ln \left(\frac{x_{B2}}{x_{B1}}\right),$ When $r_2 \rightarrow \infty$ what will be the expression for N_{Ar1} ?	(15)	210
Q9. (a) 21(b) (c)	Discuss in brief about the Equation of continuity. Explain creeping flow around the sphere. 210 210 Discuss steady state equimolar counter diffusion.	(5) (5) (5)	210

