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Total Number of Pages: 2

B.TECH
PEBT5304

5th Semester Regular / Back Examination 2015-16
BIOCHEMICAL REACTION ENGINEERING

BRANCH: BIOTECH

Time: 3 Hours

Max Marks: 70

Q.CODE: T597

Answer Question No.1 which is compulsory and any five from the rest.
The figures in the right hand margin indicate marks.

- Q1** Answer the following questions: **(2 x 10)**
- a) What do you mean by performance equation?
 - b) What are the characteristic features of an ideal reactor?
 - c) Differentiate elementary and non-elementary reactions by giving one example of each.
 - d) The pyrolysis of ethane proceeds with an activation energy of about 75000 cal. How much faster is the decomposition at 650 °C than 500 °C?
 - e) Differentiate integral method and differential method of data analysis.
 - f) Differentiate heat of solution and heat of mixing.
 - g) Write the advantages of recycling.
 - h) On doubling the concentration of reactant the rate of reaction triples. Find the order of reaction.
 - i) Define limiting reactant and excess reactant.
 - j) Write the steps of solid catalyzed reaction.
- Q2** a) Write the integral method of analysis for constant volume batch reactor operating at second order kinetics. **(5)**
- b) After 8 min in a batch reactor, reactant is 80% converted and after 18 minutes the conversion is 90%. Find the rate expression for this reaction if $C_{A0} = 1$ mol/lit. **(5)**
- Q3** a) A feed to a fractionating column analyzes by weight 30% is benzene and rest is toluene. The analysis of the distillate shows 52 weight % benzene and 4% benzene in bottom product. Calculate the amount of distillate and bottom product per 1000 kg of feed per hour. Also calculate the % recovery of benzene. **(5)**
- b) In production of SO_3 , 100 kmol of SO_2 and 100 kmol of O_2 are fed to a reactor. If the % conversion of SO_2 is 80%, calculate the composition of the product stream on mole basis. **(5)**
- Q4** . The catalytic reaction $A \rightarrow 4R$ is run at 3.2 atm and 117 °C in PFR which contains 0.01 kg catalyst and used as a feed consisting of partially converted product of 20 lit/hr of pure unreacted A The results **(10)**

are as follows

Run	1	2	3	4
C_{Ain} , mol/lit	0.1	0.08	0.06	0.04
C_{Aout} , mol/lit	0.084	0.07	0.055	0.038

Find the rate equation to represent this reaction

- Q5 a)** Gaseous reactant A decomposes as follows. **(5)**
 $A \longrightarrow 3R, -r_A = 0.6 \text{ min}^{-1} C_A$

Find the space time and conversion of A in 50% A-50% inert feed having flow rate 180 lit/min and $C_{A0}=300 \text{ mol/lit}$, to a 1 m^3 mixed flow reactor.

- b)** Write the advantages and disadvantages of fixed bed and fluidized bed reactor. **(5)**

- Q6 a)** Derive the kinetic expression for the competitive inhibition by a foreign substance **(5)**

- b)** Calculate the standard heat of formation of acetylene(C_2H_2), given that the standard heat of combustion of acetylene is -1299 kJ , the standard heat of combustion of carbon is -393.51 kJ and standard heat of formation of liquid water is -285.84 kJ . **(5)**

- Q7 a)** What are the different methods of evaluating the parameters in Michaelis-Menten equation. Derive those equations from it. **(5)**

- b)** Determine the Michaelis-Menten parameters v_m and K_m for the reaction $\text{Urea} + \text{Urease} \rightleftharpoons [\text{Urea Urease}] \rightarrow 2 \text{NH}_3 + \text{CO}_2 + \text{Urease}$ having rate constants k_1 (forward), k_2 (backward) and k_3 respectively. The rate of reaction is a function of Urea concentration as shown in the following table. **(5)**

C_{urea} , kmol/m ³	0.2	0.02	0.01	0.005	0.002
$-r_{\text{urea}}$, kmol/m ³	1.08	0.55	0.38	0.2	0.09

Finally express the rate equation for the above.

- Q8** Write short notes on any two: **(5 x 2)**

- Immobilized cell bioreactor
- Autocatalytic reaction
- Phases of cell growth
- Psychrometric chart