Registration No.												
Tot	Total number of printed pages - 02 <u>B.TECH</u>											
PCCH4301												
5 <sup>th</sup> Semester Regular / Back Examination 2015-16												
	HEAT TRANSFER BRANCH : Chemical Engineering											
	BRANCH : Chemical Engineering Time : 3 Hours											
	Max Marks : 70											
	Question Code : T159											
4	Answer Question No. 1 which is compulsory and any FIVE from the rest.											
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	ASSU	ime suitable م				-	-	ata wi ata pla		r nece	ssary.	,
1.		Answer the		-		a que.	Suona	ιι α ριο	100.		2	x 10
	(a)	The temper Explain.		• •		slab is	linear	under	stead	y state	_	
	(b)	Write the dif	ference	es betw	een co	nvectio	n and r	adiatio	n.			
	(c) In which type of boiling, radiation comes into play and why?											
	<ul> <li>(d) When Hessler's chart is used?</li> <li>(e) Differentiate between dropwise and filmwise condensation.</li> <li>(f) Differentiate between Bist number and Nuccest number.</li> </ul>											
	(f) Differentiate between Biot number and Nusselt number.											
	(g) Why impingement baffles are used in the shell and tube heat exchanger?											
	(h) Find the equivalent diameter for a triangular pitch if pitch is 1"and OD of tubes is 1.5".											
	(i)	What is radia		nape fa	ctor?							
	(j)	If a heat exc				ness =	1, what	t does t	hat me	an?		
2.	(a)	What do you equation for				ulation	of thick	ness?	Write d	lown th	е	02
	(b)	A 240mm st temperature	eam pi insula	pe, 240 ation (1	0meters K = 0	.092 \	V/m⁰C)	and	40mm	of lov	N	08
		temperature surface temp Neglect hea	peratur	es as n	neasure	ed are 3	390°C a	and 40 <sup>o</sup>	<sup>o</sup> C resp			
				heat lo								
						pipe s		rface, a	nd			
								of insu				
3.	(a)	A 100watt e	electric	bulb c	of 3cm	diame	ter is o	dumped	d unde	r soil d	of	03
		thermal con						he tem	peratu	re of th	е	
	(b)	soil 3cm dist Calculate th						lder tor	nether t	two ver	v	04
	(0)	long pieces										04
		wires are po	sitione	d vertic	ally in a	air at 20	0⁰C. He	eat tran	sfer co	efficien		
		$h = 20 W/m^2$										
	(c)	Under what effectivenes		ition, f	'ın effi	ciency	will b	e 100°	%? De	etine fi	n	03

4. (a) A counter flow concentric tube heat exchanger is used to cool 0.12 kg/s of crude oil by using cooling water at a rate of 0.18kg/s in the inner tube (ID = 20mm, OD = 40mm). The inlet and outlet temperatures of oil are 95°C and 65°C respectively. The water enters at 30°C. Neglecting tube wall resistance, fouling factor and heat loss to the surroundings, calculate the length of the tube.Data: Crude oil:  $C_p = 2131 \text{ J/Kg}^{\circ}C$ ,  $\mu$ =0.0325Ns/m<sup>2</sup>, K=0.138W/m<sup>o</sup>C

Water:  $C_p = 4174 \text{ J/Kg}^0\text{C}, \mu = 725 \times 10^{-6} \text{Ns/m}^2, \text{ K} = 0.625 \text{W/m}^0\text{C}, \text{Pr} = 4.85$ 

- (b) Draw the flow pattern in the shell side fluid using Disc and Doughnut 02 type of baffle in a shell and tube heat exchanger.
- 5. (a) A double pipe heat exchanger is employed with  $2.4m^2$  heating area to heat  $C_6H_6$  from 20°C for which water is available at 88°Cwhich flows inside the tube. Mass flow rate of  $H_2O \& C_6H_6$  are 6250 kg/hr and 5500 kg/hr. ID & OD of Inner pipe are 37.5mm and 44.8mm. ID & OD of Outer pipe are 62.5mm & 72.7mm. Find the outlet temperatures of  $C_6H_6$  and  $H_2O$  as well as find the rate of heat transfer.

	Viscosit y (cP)	K (Kcal/hr.m.°C )	Cp (kcal/kg)	ρ (kg/m³)			
H <sub>2</sub> O	0.8	0.55	1	970			
C <sub>6</sub> H <sub>6</sub>	0.57	0.138	0.4	860			

- (b) All heat exchangers cannot be condensers but all condensers can be heat exchangers. Justify this statement.
- (c) Write the enthalpy balance for the condenser operated under superheated condition with proper notations.
- A single effect, vertical short tube evaporator is used to concentrate 80 6. (a) a syrup from 10% to 40% solids at the rate of 2000 kg of feed per hour. The feed enters at 30°C and a reduced pressure of 0.33 kg/cm<sup>2</sup> is maintained in the vapour space. At this pressure, the liquor boils at 75°C. Saturated steam at 115°C is supplied to the steam chest. No sub-cooling of the condensate occurs. Calculate the steam requirement and the number of tubes (0.0254m, 16 BWG) if the height of the calendria is 1.5 m. The following data are given: Specific heat of liquor = 0.946 kcal/kg°C Latent heat of steam at 0.33 Kg/cm<sup>2</sup> = 556.5 kcal/kg Boiling point of water at this pressure = 345 K The overall heat transfer coefficient = 2150 W/m<sup>2.0</sup>C Under what condition single effect evaporator is chosen over multiple 02 (b)
  - (a) Derive Nusselt's equation for film wise condensation over a vertical
     (b) Of der what condition single effect evaporators chosen over multiple
     (c) Of der what condition single effect evaporators chosen over multiple
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- 7. (a) Derive Nusselt's equation for film wise condensation over a vertical 08 flat plate.
  (b) What is the effect of non-condensable gases during condensation? 02
- 8.Write short notes on any TWO:5 x 2
  - (a) NTU effectiveness method
  - (b) Laws of black body radiation
  - (c) Thermal boundary layer
  - (d) Analogy between heat and momentum transfer

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