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Total Number of Pages : 2

M.TECH

M.TECH 2ND SEMESTER (AR 18) REGULAR EXAMINATIONS, APRIL/MAY 2019

ADVANCED HEAT TRANSFER II

Branch: TE, Subject Code:MTEPC2020

Time: 3 Hours

Max Marks : 70

(10 X 2=20 MARKS)

PART-A

1. Answer the following questions.

- State the five methods which are available for evaluation of convection heat transfer coefficient.
- What do you mean by thermal boundary layer? How is this different from hydrodynamic boundary layer?
- State Reynolds analogy and explain its application in convective heat transfer.
- Write down two-dimensional momentum and energy equation in cylindrical coordinate system.
- What is the importance of critical heat flux?
- Write Fick's law of diffusion.
- What is the magnitude of Nusselt number for laminar flow in a tube considering constant heat flux case? What is the value of constant wall temperature plate?
- What do you mean by fouling factor?
- What are the heat transfer modes are involved in heat exchanger for heat transfer augmentation?
- State Buckingham π theorem. What are its merit and demerits?

PART-B

(5 X 10=50 MARKS)

Answer any five questions from the following.

Q.2.

- Derive the Nusselt number expression for constant heat flux case for laminar flow in tube. [5]
- With the help of Buckingham π -theorem show that for forced convection heat transfer. [5]

Q.3.

- Writing mass, momentum and energy equations, derive the Grashoff number for natural convection heat transfer using dimensionless parameters. [5]
- Air at 20°C and moving at 15 m/s is warmed by an isothermal steam heated plate at 110°C, 0.5m length and 0.5m width. Find the average heat transfer coefficient and the total heat transferred. What are heat convection coefficient, thermal boundary layer thickness and hydraulic boundary layer thickness? [5]

Q.4.

- Differentiate between Reynolds Analogy and Reynolds-Colburn Analogy. [5]
- What would be the effectiveness of counter flow heat exchanger if $C_{\min}/C_{\max}=0$ and $C_{\min}/C_{\max}=1$ [5]

Q.5.

Air at 27°C and 1 bar pressure flows over a flat plate with a velocity of 2m/s. Estimate (i) the boundary layer thickness at a distances of 20cm and 40 cm from the leading edge of the plate (ii) the mass flow that flows between $x=20$ cm and $x=40$ cm. Take μ of air at 27°C as 1.85×10^{-5} kg/ms. Assume unit depth in z-directions. If the plate is heated over its entire plate (iv) compute the drag force exerted on the first 40 cm of the plate. Properties of air at 316.5K are $\nu=17.36 \times 10^{-6}$ m²/s, $k=0.02749$ W/mK, $Pr=0.7$, $c_p=1006$ J/kgK. [10]

Q.6.

a) Show that for a parallel flow heat exchanger $\epsilon = \frac{1 - \exp[-NTU(1+R)]}{(1+R)}$ [5]

b) In the heat transfer relation $Q=UA\Delta T_{lm}$ for a heat exchanger, what is ΔT_{lm} called? Derive the expression for parallel flow heat exchanger. [5]

Q.7.

a) How is the mass transfer coefficient evaluated by dimensionless analysis. [5]

b) Air at 1 atm, 25°C, containing small quantities of iodine flows with a velocity of 5.18 m/s inside a 3.048 cm diameter tube. Determine the mass transfer coefficient for iodine transfer from the gas stream to the wall surface. If C_m is the mean concentrate of iodine in kg mol/m³. In the air stream, determine the rate of deposition of iodine on the tube surface where the iodine concentration is zero. Take kinematic viscosity of air is 1.58×10^{-5} m²/s and D for air-iodine system at 1 atm, 298K is 0.826×10^{-5} m²/s. [5]

Q.8. Write short notes on:

a) Equimolar counter diffusion [5]

b) Fick's law of diffusion [5]

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