

GIET MAIN CAMPUS AUTONOMOUS GUNUPUR – 765022

R4A19001097

| Registration No: | | | | | | | | | | | | | |
|--|---|---------------|-----------|------------|----------|---------|---------|------------|------------|------------------|------------|--|--|
| Total N | Number of Pages | : 2 | | | | | | | | B. | ГЕСН | | |
| 4 th Semester Regular Examination-April-May 2019 | | | | | | | | | | | | | |
| BBTPC4040 – BIOCHEMICAL REACTION ENGINEERING | | | | | | | | | | | | | |
| (Regulations 2017) Biotech Branch | | | | | | | | | | | | | |
| Time : 3 Hours Maximum : 100 Marks Answer ALL Questions | | | | | | | | | | | | | |
| The figures in the right hand margin indicate marks. | | | | | | | | | | | | | |
| PART – A: (Multiple Choice Questions) 10 x 2=20 Mark | | | | | | | | | | | | | |
| Q.1. Answer <u>All</u> Questions. | | | | | | | | | | | | | |
| a | If 100 moles of hydrogen fed to a reactor with oxygen for the production of 80 moles of [CO1][PO2 | | | | | | | | | [CO1][PO2] | | | |
| | water, the amount of oxygen required is moles. | | | | | | | | | | | | |
| _ | a). 80 b) 60 c) 40 d) 20 | | | | | | | | | | | | |
| b | The temperature measured by keeping dry the bulb of a thermometer is | | | | | | | | | [CO1][PO1] | | | |
| 0 | a) less than DBT b) more than DBT c) more than WBT d) less than WBT Molal humidity $= - \times A$ becaute humidity | | | | | | | | | | [CO2][PO1] | | |
| c | Molal humidity = $_$ × Absolute humidity. a) 18/29 b) 29/18 c) 18 d) 29 | | | | | | | | | | | | |
| d | | | | | | | | | | | | | |
| | a) adiabatic reaction b) isothermal reaction c) exothermic reaction d)endothermic reaction | | | | | | | | | ermic reaction | [CO2][PO1] | | |
| e | For obtaining the | - | | m concer | ntratio | n vs. t | ime d | ata by | v assu | ming the order | [CO2][PO1] | | |
| | of reaction, the m | | | | | | | | | | | | |
| | a) integral analys | |) differe | ntial ana | lysis m | nethod | c) bo | th inte | egral a | and differential | | | |
| f | methods d) nor A zero order rea | | R) with | rate cor | netant 1 | | ure in | n a hat | ch re | actor Find the | [CO2][PO2] | | |
| 1 | | | | | | | | | | | | | |
| | time required to achieve 50 % conversion with initial concentration of reactant 10 mol/lit. a) 10 b) 5 c) 1.0 d) 0.5 | | | | | | | | | | | | |
| g | For gas phase rea | | - | | | - | | s. | | | [CO2][PO1] | | |
| | a) PFR b)MFR c)both i and ii d)none of these | | | | | | | | | | | | |
| h For a reaction whose rate expression is $-r_A = 3.123 C_A^{1.75}$, the volume of PFR required times the volume of MFR for a fixed conversion. | | | | | | | | | | [CO2][PO2] | | | |
| | | b) 1.0 c)1. | | | 1001510 | 11. | | | | | | | |
| i | Double time of c | , , | , | | owth r | ate). | | | | | [CO3][PO1] | | |
| | a) 0.893 b) 0.693 c) 0.493 d)0.293 | | | | | | | | | | | | |
| j | For autocatalytic reaction is best option for continuous process. a) batch reactor b) PFR c)MFR d) recycle reactor | | | | | | | | [CO2][PO1] | | | | |
| | a) bat | ch reactor b) |) PFR c) | MFR d) 1 | recycle | reacto | or | | | | | | |
| | | PART – I | R• (Shor | t Answe | r Oue | stions |) 2x1(|)-20 N | Mark | e | | | |
| Q.2. | Answer <u>ALL</u> q | | | | I Que | Stions | / =/110 | 01 | ·141 IX | 0 | | | |
| a | What is the diff | | een disti | llation ar | nd evap | oratio | n oper | ration | ? | | [CO1][PO1] | | |
| b | Define absolute humidity and molal humidity. | | | | | | | | [CO1][PO1] | | | | |
| c | | | | | | | | | | [CO1][PO2] | | | |
| | components have the specific heat of 10, 20, and 30 kcal/kg.K for H_2 , N_2 , and O_2 | | | | | | | | | | | | |
| d | respectively, cal | | pmix• | | | | | | | | [CO2][PO1] | | |
| e | Define rate of reaction. Rate of reaction is a function of and | | | | | | | | [CO2][PO1] | | | | |
| f | Define Arrhenius equation for reaction rate constant. | | | | | | | | | [CO2][PO2] | | | |
| g | | | | | | | | | | [CO3][PO2] | | | |
| h | Define Michaelis-Menten (K_m) constant. [CO2 | | | | | | | | | [CO2][PO2] | | | |
| i | Define standard | | | | | | | | | | [CO2][PO1] | | |
| j | j Define limiting and excess reactant. [CO1][PO2] | | | | | | | | | [CO1][PO2] | | | |
| | | | | | | | | | | | | | |



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PART – C: (Long Answer Questions) 15x4=60 Marks

| | TART C. (Long Answer Questions) 1544–00 Marks | | | | | | | |
|--|---|------------|------------|--|--|--|--|--|
| Q.3 | 3 | | | | | | | |
| a. | What is the amount of water evaporated and thick liquor produced when 10,000 kg/hr aqueous feed solution of 10 % solid (by weight) is concentrated to 40 % solid (by weight) ? | 3 | [CO1][PO1] | | | | | |
| b. | Derive the expression for the rate of product formation for the reversible uncompetitive enzyme inhibition and show the result in Line-Weaver-Burk plot. | 12 | [CO3][PO2] | | | | | |
| | OR | | | | | | | |
| c. | Derive the expression for the rate of product formation for the reversible competitive enzyme inhibition and show the result in Line-Weaver-Burk plot. | 10 | [CO3][PO2] | | | | | |
| d. | Calculate the heat of reaction at 298.15 K of the following reaction: | | [CO1][PO1] | | | | | |
| $C_2H_6(g) \rightarrow C_2H_4(g) + H_2(g)$ | | | | | | | | |
| | Data: | | | | | | | |
| | Component ΔH^{o}_{C} , (kJ/mol) | 5 | | | | | | |
| | C ₂ H ₆ -1560.69 | | | | | | | |
| | C ₂ H ₄ -1411.2 | | | | | | | |
| | H ₂ -285.83 | | | | | | | |
| Q.4 | 4 | | | | | | | |
| a. | Derive Michaelis-Menten equation for the enzyme catalyzed reaction. | 7 | [CO3][PO2] | | | | | |
| b. | Explain the factors affecting the enzyme activity. | 8 | [CO3][PO1] | | | | | |
| | OR | | | | | | | |
| c. | Draw a Psychrometric chart and explain its importance. | 8 | [CO1][PO2] | | | | | |
| d. | Explain the different phases of cell growth. | 7 | [CO3][PO1] | | | | | |
| Q.5 | | | | | | | | |
| Q. . a. | | [CO2][PO2] | | | | | | |
| а. | Derive an expression for C_{Rmax} , in a series reaction of $A \rightarrow R \rightarrow S$, with the rate constants for first order reactions K_1 and K_2 are 5 and 2 min ⁻¹ respectively. | 12 | | | | | | |
| b. | Find the maximum time for C_{Rmax} , in a series reaction of $A \rightarrow R \rightarrow S$, with the rate | 3 | [CO2][PO1] | | | | | |
| | constants for first order reactions K_1 and K_2 are 5 and 2 min ⁻¹ respectively. | 3 | | | | | | |
| | OR I J | | | | | | | |
| c. | Explain the volume comparison of CSTR and PFR with the help of $1/(-r_A)$ vs. X _A plot | 10 | [CO3][PO2] | | | | | |
| | and V_{MFR}/V_{PFR} vs. 1-X _A plot, for +ve and 0 order reactions. | 10 |][] | | | | | |
| d. | Draw a plot of $1/(-r_A)$ vs. X_A for -ve order reaction and comment on volume required | - | [CO3][PO1] | | | | | |
| | by MFR and PFR for a fixed X_A . | 5 | | | | | | |
| Q.6 | • | | | | | | | |
| a. | Derive an expression relating the volume of PFR and conversion and show in $1/(-r_A)$ | 0 | [CO3][PO1] | | | | | |
| | vs. X _A plot. | 8 | [] | | | | | |
| b. | A zero order reaction (A \rightarrow R) with rate constant 10 occurs in a plug flow reactor. | | [CO2][PO1] | | | | | |
| 0. | Find the volume required to achieve 90 % conversion with initial concentration of | 7 | [00]][101] | | | | | |
| | reactant 100 mol/lit and volumetric flow rate of reactant 25 lit/min. | | | | | | | |
| OR | | | | | | | | |
| c. | | | [CO3][PO1] | | | | | |
| . | Derive the performance equation of a recycle reactor. | 10 | | | | | | |
| d. | Show the performance equation of a recycle reactor in $1/(-r_A)$ vs X _A . | 5 | [CO3][PO1] | | | | | |
| | | 5 | | | | | | |

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