QP Code: RA22BTECH396	Reg.						AR 22

## Gandhi Institute of Engineering and Technology University, Odisha, Gunupur (GIET University)



Time: 3 hrs

B. Tech (Sixth Semester - Regular) Examinations, April 2025

## 22BCHPC36001 – Process Equipment Design (Chemical)

Maximum: 70 Marks

(Chemical)

(The figures in the right hand margin indicate marks)
Graph paper and databook are allowed with proper verification

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PART – A	$(2 \times 5 =$	10 Ma	rks)
Q.1. Answer ALL questions		CO#	Blooms Level
a. What is the role of design Engineer in plant design?		CO1	K1
b. What do you mean by 25% cut segmental baffle?		CO3	K1
c. What is the q-line slope value of super saturated vapor feed?		CO2	K1
d. What are the main factors considered when designing the diameter of an absorption	tower?	CO2	K2
e. Why is the choice of material important in storage tank design?		CO4	K2
PART – B	15 x 4 =	60 M	arks)
Answer All the questions	Marks	CO#	Blooms Level
2. a. A feed mixture containing 50 mole % benzene and rest toluene is to be separated into an overhead product containing 93 mole % benzene and a residue of 3 mole % benzene at 1 std. atm. Feed is saturated liquid and is admitted to the column at the rate of 100 tons/day. A reflux ratio of 3.5 is to be used. Boiling point of benzene and toluene are 353 K and 383 K, respectively. Relative volatility for benzene-toluene system is 2.3. Vapor velocity can be taken as 1 m/s. Design a suitable sieve tray distillation column.	15	CO2	K3
b. A counter current packed tower is used to separate ammonia from coke oven gas by employing water as solvent. Inlet gas contains 25% ammonia at a rate of 158 kmol/hr. Outlet gas liquid contain 1.5% and 18% ammonia after recovery (all are in mole%). Calculate the packing height required if mass transfer co-efficient is 135 kmol/hr.m². Equilibrium relation is: y = 2.6x, where x & y are mole fractions of ammonia in liquid and gas phase.	15	CO2	К3
3.a. Design a horizontal shell & tube Heat Exchanger to heat $10000 \text{kg/hr}$ of water to $66^{\circ}\text{C}$ by condensing the steam at 1.4bar absolute pressure on the shell side. The raw water is available at $21^{\circ}\text{C}$ . Brass tube (k= 85.5W/m. k) having 25.4mm outside diameter and 22.1mm inside diameter are to be used on a 37.5mm triangular pitch. Tubes should not be longer than 2500mm. To reduce pressure losses due to friction a low water velocity of 30.5cm/sec might be used. Effect of the tube fouling, shell side fluid distribution may be neglected. The condensing film coefficient is given by:  NuCondensation = $0.725(\frac{g\rho^2D_0^3}{\mu k\Delta t})^{1/4}$ Water film coefficient is given by: Nu = $0.023(\text{Re})^{0.8}(\text{Pr})^{0.4}$	15	CO3	К3
(OR)			
b. Design a horizontal tube single effect evaporator to concentrate 6000 kg/hr of 8%	15	CO3	К3

(by weight) caustic soda solution to 20% (by weight). Steam is available at 1.9

kg/cm<sup>2</sup>. The pressure to be maintained in the vapour space of the evaporator is 400 mm Hg. The overall heat transfer co-efficient may be taken as 3000 kcal/hr.m<sup>2</sup>.°C. Boiling point elevation of the solution is 10°C. Enthalpy of the feed and product streams are 90 and 79 kcal/kg, respectively. Tubes of 50 mm OD (45 mm ID) and length of 150 cm are arranged in 75 mm square pitch.

4.a. Design a shell for storage vessel with at least two different thickness sheets: Data:

15 CO4 K3

Tank diameter	25 m
Tank height	20 m
Specific gravity of liquid	0.8
Material	Carbon steel (Structural)
Permissible stress	142N/mm <sup>2</sup>
Density	7.7
Modulus of elasticity	2*10 <sup>5</sup>

(OR)

b. 1) Design a shell, head and flange of a pressure vessel.

15 CO4 K3

Data:

Shell: <u>Head:</u>

ID: 1200mm

Material: Stainless steel

Permissible stress (150°C):130

N/mm²

Kunckle radius: 72mm

Internal pressure: 0.3 N/mm²

Material: Same as shell

Flanges: Bolts:

Material: Carbon steel Material: Hot rolled carbon

Permissible stress (250°C): 95 N/mm<sup>2</sup> steel

Gasket: Asbestos Permissible stress (50°C):

Nominal diameter: 1200mm 58.7N/mm<sup>2</sup>

Inside diameter of flange: 1202mm Permissible stress (200°C):

Outside diameter of flange: 1315mm 54.5N/mm<sup>2</sup>

Outside diameter of stainless steel lining ring (raised face): 1240mm Bolt circle diameter: 1270mm Thickness of flange: 45mm

Number of Bolt: 48

5.a. Draw a neat diagram of plate distillation column showing all the important 8 CO2 K2 accessories & different types of plates.

b. Draw a neat diagram of storage vessel showing all the important accessories and 7 CO4 K2 tori spherical dished head.

(OR)

- c. Draw a neat diagram of Calendria evaporator showing all the important 8 CO3 K2 accessories and neat label.
- d. Draw a neat diagram of double pipe heat exchanger showing all the important 7 CO3 K2 accessories and with hair pin.

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