QP Code: RN22BTECH273 Reg. No

Gandhi Institute of Engineering and Technology University, Odisha, Gunupur (GIET University)



B. Tech (Fifth Semester - Regular) Examinations, November - 2024

22BCHPC35004 - Mass Transfer-II

(Chemical Engineering)

EXCELLENC	e - OUR GRAPHICE			()	Chemical	Engineer	ring)				
Tiı	me: 3 hrs		Max						ximum: 70 Marks		
					r ALL que			,			
(The figures in the right hand margin indicate marks) PART – A								2 x 5 =	10 Ma	rlza)	
ra.	KI – A							(2 x 3 =	TU IVIA	irks)
Q.1. A	answer ALL	questions								CO#	Blooms Level
a. I	a. Differentiate between stage type and differential extractor.									CO1	K1
b. I	Define decoction, elution and lixiviation in leaching.									CO2	K1
c. V	Vrite Mier's	supersatu	ration theor	y.						CO2	K1
d. I	Differentiate	between p	hysical and	d chemical	adsorption	•				CO3	K1
e. V	Write the ap	plication of	f spray drye	er.						CO4	K1
$\mathbf{PART} - \mathbf{B}$									$15 \times 4 = 60 \text{ Marks}$		
Answe	er All the qu	<u>iestions</u>							Marks	CO#	Blooms Level
2. a.	1000 kg/hı	of a nicot	ine-water s	olution co	ntaining 1%	nicotine i	s to be extr	acted	10	CO1	K3
	_				tent to 0.19						
	immiscible	e solvents.	What is th	e minimur	n solvent r	equiremen	t, kg/hr? If	1150			
	kg/hr of so	lvent is us	ed, how ma	ny theoret	ical stages	are require	d?				
	X,	0	0.00101	0.00246	0.00502	0.00998	0.0204				
	y,	0	0.00087	0.00196	0.00456	0.00913	0.0187				
b.	Explain the	e selection	criteria of	solvent for	proper ext	raction.			5	CO1	K2
	b. Explain the selection criteria of solvent for proper extraction. (OR)										
c.	25% of die	oxane in w	ater solution	, ,	kg is to be	extracted	with benze	ene to	10	CO1	К3
	25% of dioxane in water solution of 1000kg is to be extracted with benzene to remove 95% of dioxane. If the extraction were done with equal amount of										
	solvent in 5 cross current stages, how much solvent would be required?										
	X,										
	Y'		0.0548		0.29		0.47				
d.	Describe a	bout perfor	rated plate	column in	details with	neat sket	ch.		5	CO1	K2
3.a.	Seeds con	taining 20	% by weig	tht oil are	to be extr	acted in a	counter-ci	ırrent	10	CO2	КЗ
	plant and 9	90% of the	oil is recov	ered in a s	solution cor	ntaining 50	% by weigl	nt oil.			
	If the seed	s are conta	cted with	fresh solve	ent and 1 kg	g of solution	on is remov	ed in			
	the underf	low in asso	ociation wi	th every 21	kg of inso	luble matte	er, determin	ne the			
	theoretical	stages req	uired?								
b.									5	CO2	K2
				(OR)							
c.	Crushed of	il seeds cor	ntaining 55	% oil by w	eight are to	o be extrac	ted at the r	ate of	10	CO2	К3
			_	•	containing						
	_	_	_		on system i	-	_				
			-		Calculate t						
	_	1	-			•	•				

	obtained under above conditions.			
d.	Describe about Bollman extractor in details with neat sketch.	5	CO2	K2
4.a.	The equilibrium water adsorbed by a silica gel in contact with moist air varies with the humidity of air, as: $Y=3.5*10^{-2} X$.	10	CO3	К3
	Where X= kg water adsorbed/kg of dry gel, Y= humidity of air, kg moisture/kg			
	dry air.			
	0.5 kg silica gel containing 6% (dry basis) adsorbed water is placed in a			
	collapsible vessel in which there are 9 m ³ of moist air, the partial pressure of			
	water being 15 mm Hg. The total pressure and temperature are kept at 1 atm and			
	298 K. Calculate the amount of water picked up from the moist air in the vessel			
	by silica gel.			
b.	Explain the methods of crystallization.	5	CO3	K2
	(OR)			
c.	Experiments on decolorisation of oil yielded the following equilibrium	10	CO3	К3
	relationship:			
	$y=0.5x^{0.5}$			
	Where $y = gm$ of color removed/gm of adsorbent			
	x = color in oil, gm of color/1000gm of color-free oil			
	100 kg of oil containing 1 part of color to 3 parts of oil is agitated with 25kg of			
	the adsorbent. Calculate the % of color removed if: All 25kg adsorbent is used			
	in one step. 12.5 kg adsorbent is used initially, followed by another 12.5kg of			
a	adsorbent.	_	CO3	К2
d.	Describe in details about Swanson Walker Crystallizer.	5	CO3	
5.a.	Slabs of paper pulp 100*100*1.5cm ³ are to be dried under constant drying conditions from 67% to 30% moisture. The value of equilibrium moisture for	10	CO4	К3
	the material is 0.5%. If critical moisture is 60% and rate of drying at critical			
	point is 1.5kg/m ² hr, calculate the drying time. The dry weight of each slab is			
	2.5kg. Drying is taking place in 2 big faces of the slab. All the moisture contents			
	are on wet basis. The falling rate may be assumed to be linear.			
b.	Explain rate of drying with suitable plot.	5	CO4	K2
0.	(OR)			
c.	Derive the total time of drying.	8	CO4	К3
d.	Describe in details about drum dryer.	7	CO4	K2
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